

Supporting Information

Mixed matrix membranes based on metal-organic frameworks with tunable pore size for CO₂ separation

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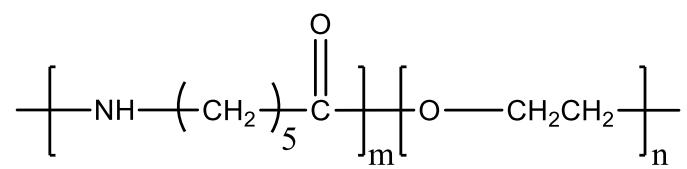


Figure S1 The structural formula of the polymer Pebax used in this work.



Figure S2 Optical image of the pure polymer Pebax membrane.

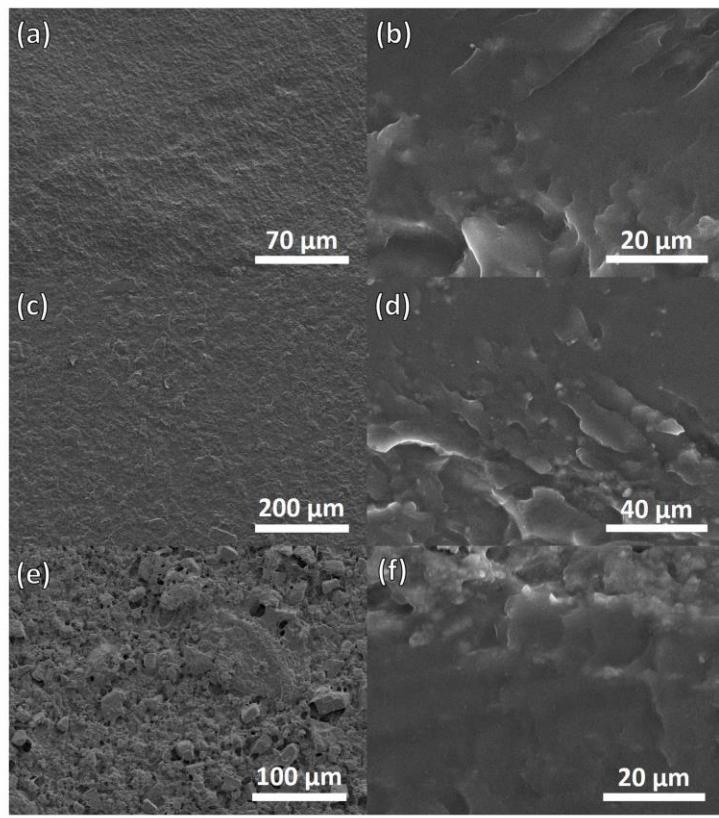


Figure S3 Top view and cross-section SEM images of (a) (b) $\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-10}$, (c) (d) $\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-20}$ and (e) (f) $\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-30}$.

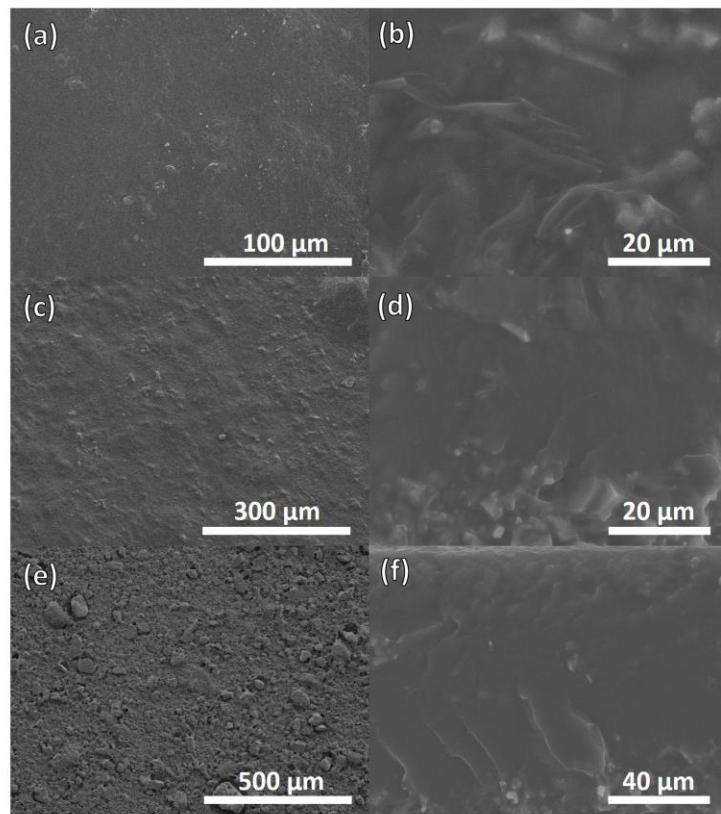


Figure S4 Top view and cross-section SEM images of (a) (b) $\text{Ni}_2(\text{L-asp})_2\text{pz}@\text{Pebax-10}$, (c) (d) $\text{Ni}_2(\text{L-asp})_2\text{pz}@\text{Pebax-20}$ and (e) (f) $\text{Ni}_2(\text{L-asp})_2\text{pz}@\text{Pebax-30}$.

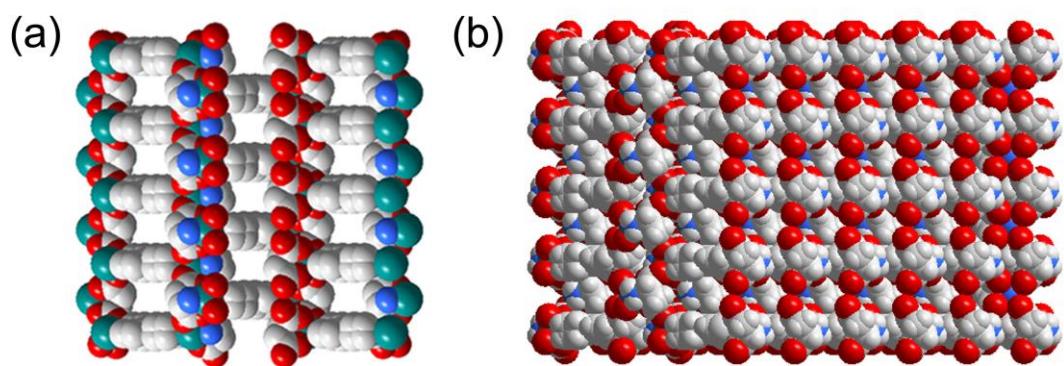


Figure S5 3D structure of $\text{Ni}_2(\text{L-asp})_2\text{bipy}$ (Ni cyan, C gray, N blue and O red;) viewed along (a) $[0 \ 1 \ 0]$ and (b) $[1 \ 1 \ 0]$.

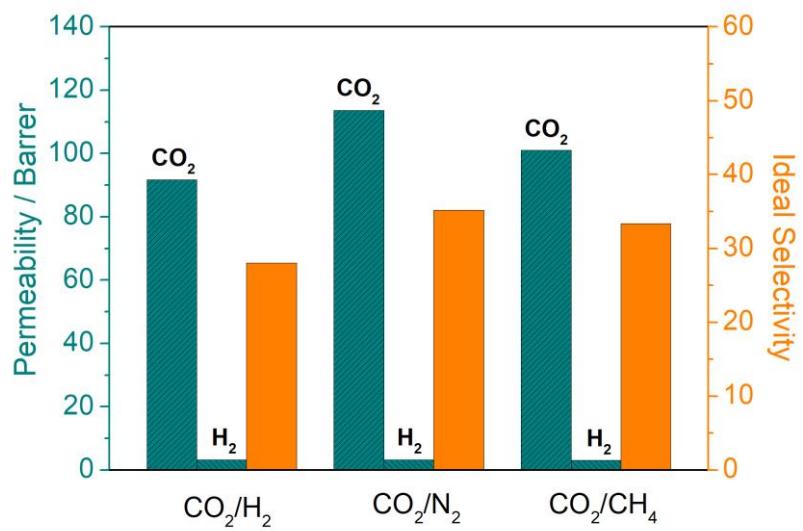


Figure S6 The binary gas mixture (CO_2/H_2 , CO_2/N_2 and CO_2/CH_4) permeability and corresponding selectivity of $\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-20}$ membrane.

Table S1 Pure component CO₂, H₂, N₂ and CH₄ permeation properties of Ni₂(L-asp)₂bipy@Pebax membranes measured at 1 atm pressure and 25 °C.

Membrane	Permeability (Barrer)				Selectivity		
	CO ₂	H ₂	N ₂	CH ₄	CO ₂ /H ₂	CO ₂ /N ₂	CO ₂ /CH ₄
Pebax	55.85	32.11	1.39	1.56	1.729	40.18	35.81
Ni ₂ (L-asp) ₂ bipy@Pebax-10	107.5	5.427	4.571	5.004	19.81	23.52	21.48
Ni ₂ (L-asp) ₂ bipy@Pebax-20	120.2	3.656	3.052	3.243	32.88	39.38	37.06
Ni ₂ (L-asp) ₂ bipy@Pebax-30	82.31	2.72	1.571	2.353	30.26	52.39	34.98

Table S2 Pure component H₂ CO₂ N₂ and CH₄ permeation properties of Ni₂(L-asp)₂pz@Pebax membranes measured at 1 atm pressure and 25 °C.

Membrane	Permeability (Barrer)				Selectivity		
	CO ₂	H ₂	N ₂	CH ₄	CO ₂ /H ₂	CO ₂ /N ₂	CO ₂ /CH ₄
Pebax	55.85	32.11	1.39	1.56	1.729	40.18	35.81
Ni ₂ (L-asp) ₂ pz@Pebax-10	46.10	4.603	2.487	3.820	10.01	18.54	12.07
Ni ₂ (L-asp) ₂ pz@Pebax-20	89.66	2.896	3.105	3.875	30.96	28.88	23.14
Ni ₂ (L-asp) ₂ pz@Pebax-30	80.83	2.478	2.662	3.431	32.62	30.36	23.56

Table S3 Binary gas mixture (CO_2/H_2 , CO_2/N_2 and CO_2/CH_4) permeation properties of $\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-20}$ membrane measured at 1 atm pressure and 25 °C.

Membrane	Permeability (Barrer)						Selectivity		
	CO_2/H_2		CO_2/N_2		CO_2/CH_4		CO_2/H_2	CO_2/N_2	CO_2/CH_4
	CO_2	H_2	CO_2	N_2	CO_2	CH_4			
$\text{Ni}_2(\text{L-asp})_2\text{bipy}@\text{Pebax-20}$	91.7	3.27	113.6	3.23	101.0	3.03	28.04	35.17	33.33

Table S4 Comparison of gas separation performance of this work with those of reported MOF based MMMs.

membrane	Temp	Pressure (bar)	Loading	CO ₂ permeability	CO ₂ /H ₂	CO ₂ /N ₂	CO ₂ /CH ₄	reference
Pebax-1657/4A Zeolite	25	24.5	10%	97	-	54	26.5	[1]
Pebax-1657/4A Zeolite	25	24.5	30%	155.8	-	12.9	7.9	[1]
Pebax-1657/GTA	25	4	80%	1200	29	51	9	[2]
IL-Pebax-1657/ZIF-8	30	2	8%	261	10	71	36	[3]
Pebax/PDA/ZIF-8-15 (dry)	25	1	15%	220.06	-	56.14	-	[4]
Pebax/PDA/ZIF-8-15 (humidified)	25	1	15%	267.74	-	62.65	-	[4]
MWCNTs/Pebax	30	10	5%	265.15	6.4	58.5	-	[5]
MWCNTs/Crosslingked Pebax	30	10	5%	17.47	2.4	84.5	-	[5]
[bmim][Tf2N]/ZIF-8/Pebax 1657	25	1	15%	104.9	10	83.9	34.7	[6]
UiO-66-PEBA (humid)	25	3	10%	139.7	-	61.1	-	[7]
UiO-66-PEBA-NH2 (humid)	25	3	10%	130.2	-	72.2	-	[7]
ZIF-7/Pebax-1657	25	3.75	22%	111	-	97	30	[8]
Pebax-1657/PEG50	30	0.6	50%	151	10.8	47	15.5	[9]
Pebax-1657/PEG-DME	30	0.3	50%	606	15.1	43	-	[10]
Pebax/CuBTC/PEG-ran-PPG	30	15	32.76% (PEG-ran-PPG) /20% (CuBTC)	1163.8	-	-	32.7	[11]
(Pebax1657)/S APO-34	35	7	50%	338	9	54	18	[12]
Pebax	25	1	-	50.5	6.38	79.5	16.7	This work
Ni ₂ (L-asp) ₂ bipy @ Pebax-20	25	1	20%	120.2	32.88	39.38	37.06	This work

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