

## **SUPPORTING INFORMATION**

### **The Role of Isolated Acid Sites and Influence of Pore Diameter in the Low-Temperature Dehydration of Ethanol**

Matthew E. Potter,<sup>†\*</sup> Mary E. Cholerton,<sup>†</sup> Julija Kezina,<sup>†</sup> Richard Bounds,<sup>†</sup> Marina Carravetta,<sup>†</sup> Maela Manzoli,<sup>‡</sup> Enrica Gianotti,<sup>‡</sup> Michael Lefenfeld,<sup>‡</sup> and Robert Raja<sup>†\*</sup>

<sup>†</sup>School of Chemistry, University of Southampton, University Road, Southampton, SO17 1BJ, United Kingdom

<sup>‡</sup>Department of Chemistry & NIS-Interdepartmental Centre, University of Turin, Via P. Guiria, 10125, Torino, Italy

<sup>‡</sup>Dipartimento di Scienze e Innovazione Tecnologica, Centro Interdisciplinare Nano-SiSTeMI, Università del Piemonte Orientale, Via T. Michel 11, 15100, Alessandria, Italy

<sup>‡</sup>SiGNa Chemistry Inc, 845 Third Avenue, Suite 623, New York City, New York 10022, United States

Corresponding authors Email: M.E.Potter@soton.ac.uk, R.Raja@soton.ac.uk

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## **Experimental details**

### **Catalysis synthesis**

The SAPO-34 and SAPO-5 synthesis were prepared according to references 1-3. Key ingredients and synthetic conditions are listed below in Table S1.

In both cases the as-prepared samples were calcined in a tube furnace under a flow of air at 575 °C for 16 hours yielding a white solid.

	SAPO-5	SAPO-34
Aluminium source	Aluminium hydroxide hydrate (Aldrich)	Aluminium isopropoxide (Aldrich)
Silicon source	Silica sol (40 wt% in H <sub>2</sub> O, Aldrich)	Fumed silica (Aldrich)
Structure directing agent	Triethylamine (Fisher)	Tetraethylammonium hydroxide (35 wt% in H <sub>2</sub> O, Aldrich)
Crystallization temperature/ °C	180	200
Crystallization time/ h	24	60

**Table S1:** Summary of synthetic conditions.

### **Characterisation**

ICP-OES measurements were performed by Medac.

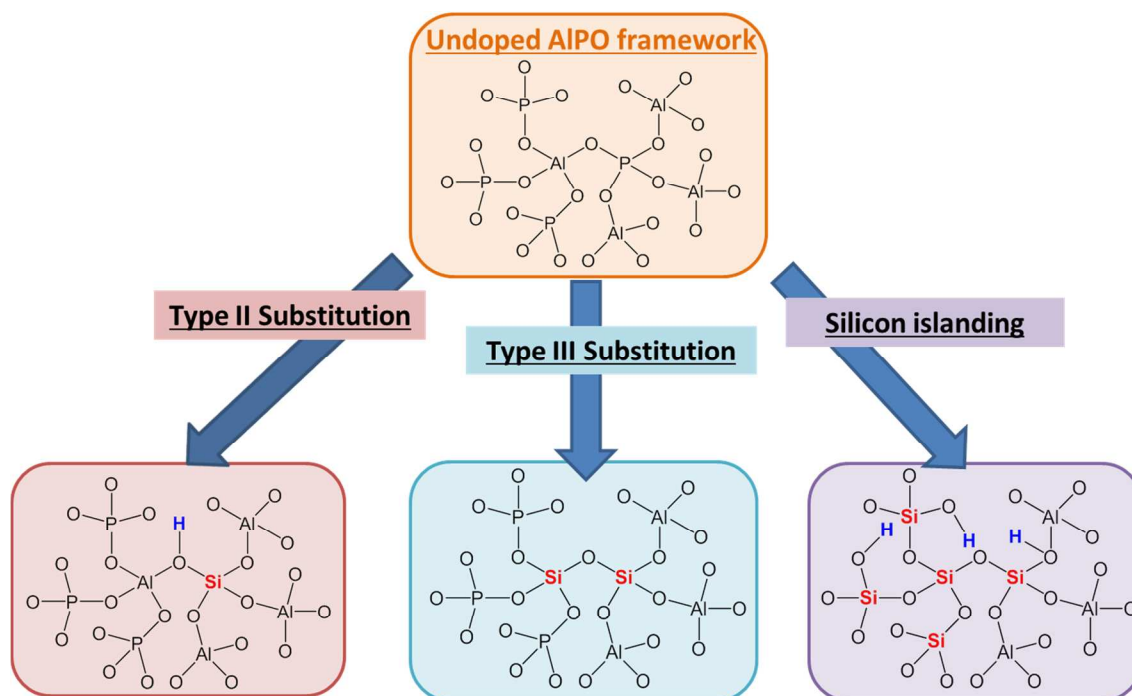
Phase purity and crystallinity of materials was confirmed by powder X-ray diffraction. Powder X-ray diffraction (PXRD) was carried out using a Bruker D2 Phaser diffractometer using Cu K<sub>α1</sub>/K<sub>α2</sub> radiation  $\lambda = 1.5418 \text{ \AA}$ , PXD patterns were run over a  $2\theta$  range of 5-45° with a scan speed of 3° min<sup>-1</sup> and increment of 0.01°.

Scanning electron microscopy was carried out using a Jeol JSM-5910.

### **Catalysis**

Catalysis was performed using a custom build flow reactor provided by Cambridge Reactor Design. The reactor comprised of a syringe pump, laptop computer, two mass flow controllers, reactor with heater and control box. A 224 mm quartz reactor tube (4 mm id, 6 mm od) with a 4 mm high frit 80 mm from the base of the tube and a gas inlet 25.8 mm from the top was placed inside the heater jacket. Liquid and gas flows were controlled using a Harvard Apparatus Model 33 MA1-55-3333 syringe pump and Brooks IOM585OS mass flow controller respectively and flow rates were input via computer interface.

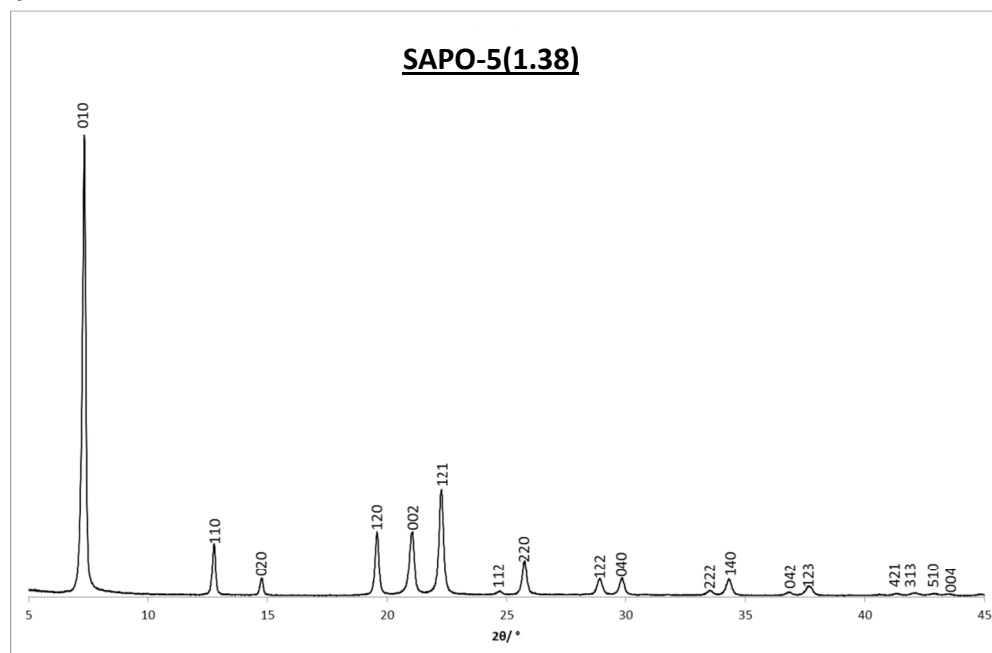
## Silicon substitution mechanisms



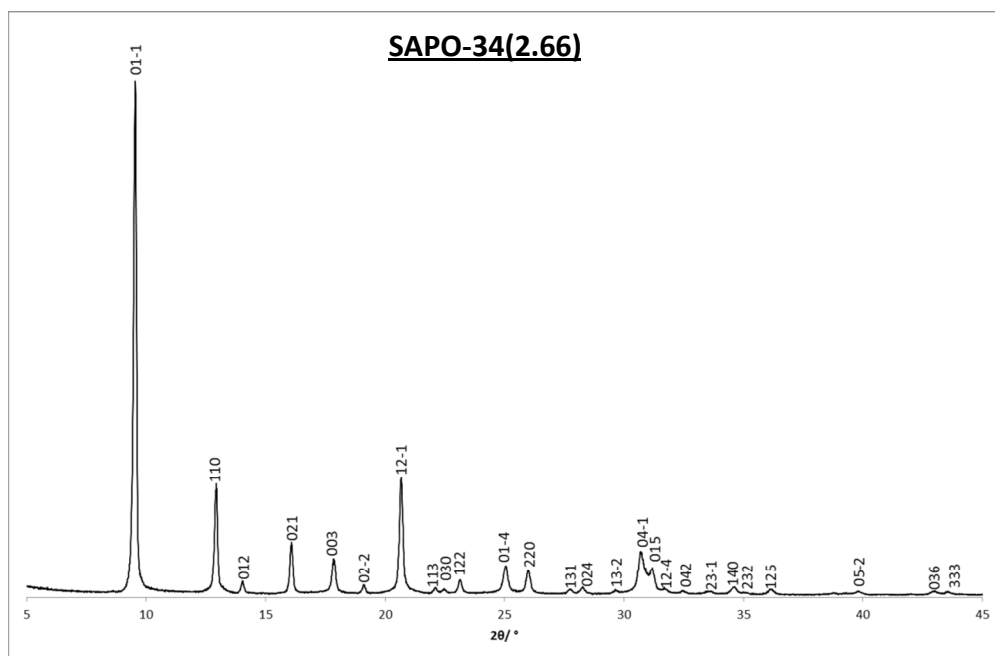
**Figure S1:** Possible silicon substitution methods into an AlPO framework.

## Textural characterization results

### Powder X-ray diffraction



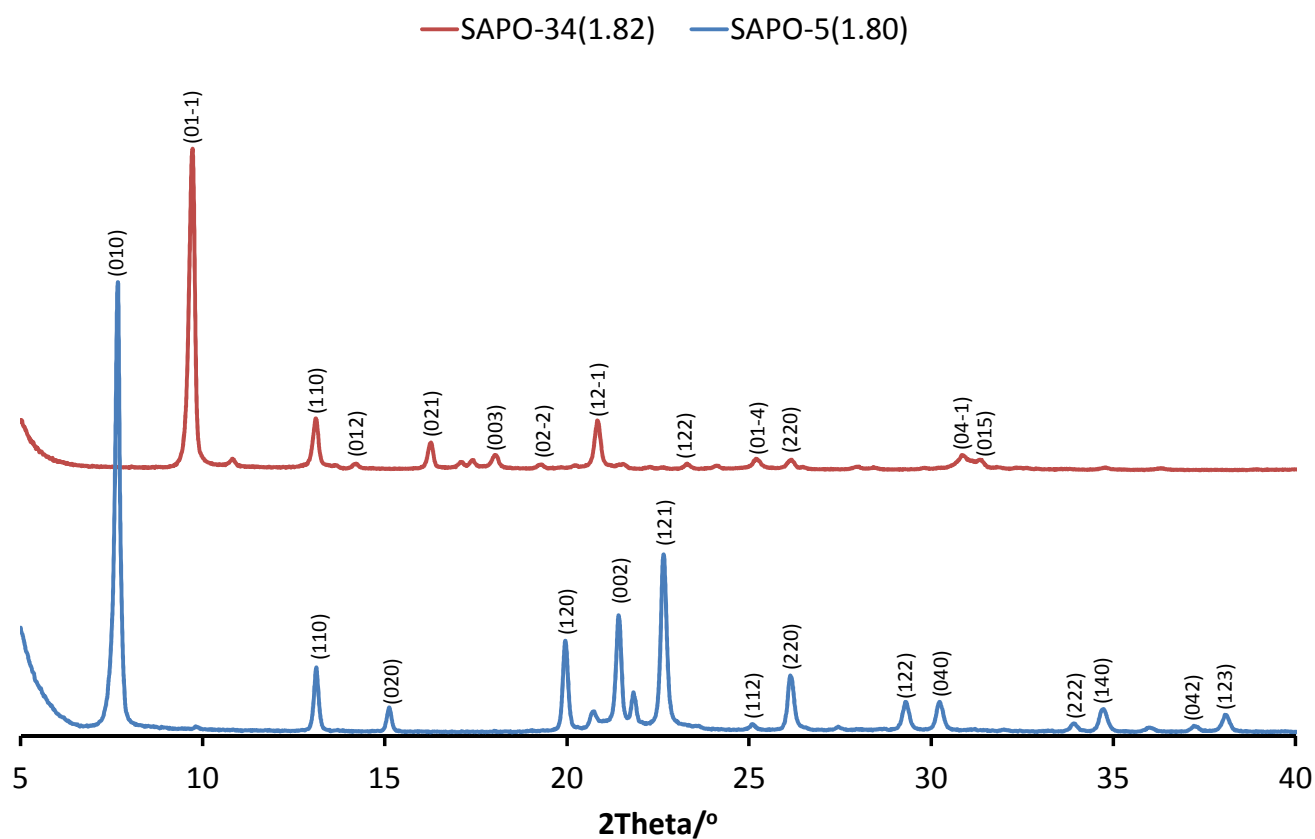
**Figure S2:** Powder X-ray diffraction pattern for phase-pure SAPO-5(1.38).



**Figure S3:** Powder X-ray diffraction pattern for phase-pure SAPO-34(2.66).

Catalyst	Alpha/ Å	Gamma/ Å	Volume/ Å <sup>3</sup>
SAPO-5(1.38)	13.8431	8.4295	1398.93
SAPO-34(2.66)	13.7097	14.9052	2426.20

**Table S2:** Unit cell data for SAPO-5 and SAPO-34 as determined using Celref.<sup>[4]</sup>



**Figure S4:** Powder XRD patterns for SAPO-34(1.82) and SAPO-5(1.80) showing main phase.

#### BET surface area measurements

	SAPO-5(1.38)	SAPO-34(2.66)
BET surface area/ $\text{m}^2\text{g}^{-1}$	250.98	479.37

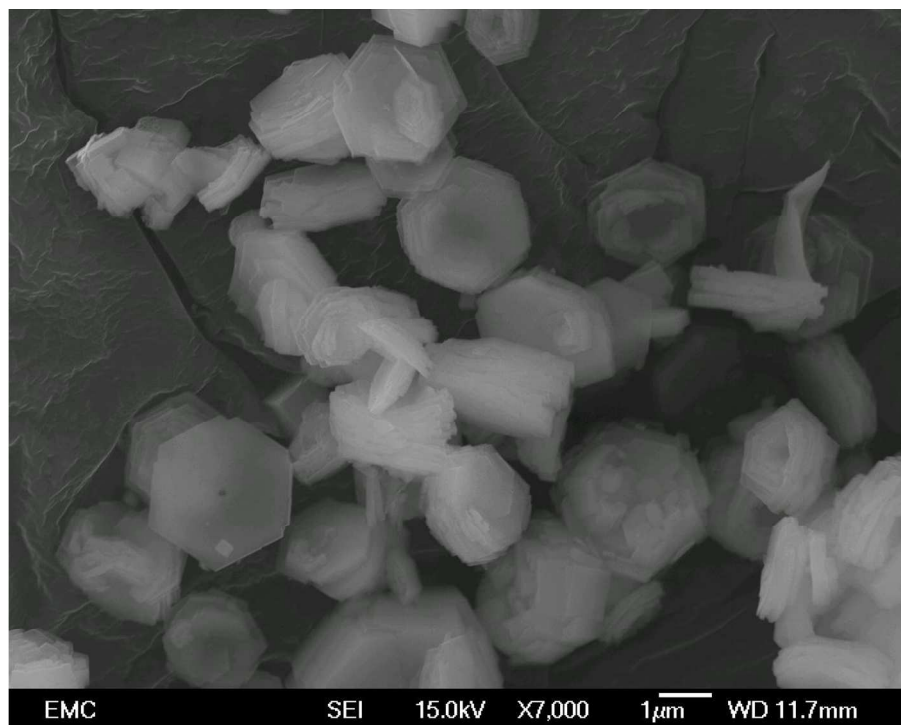
**Table S3:** Surface area measurements determined using BET.

#### Crystallite size calculations

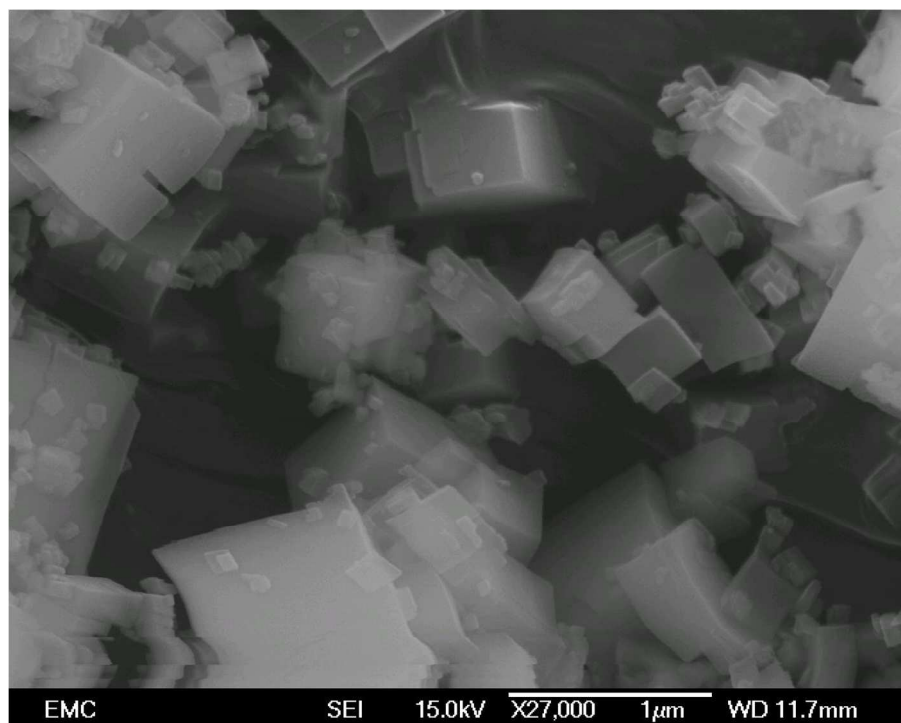
	SAPO-34(2.66)	SAPO-34(1.82)	SAPO-5(1.80)	SAPO-5(1.38)
Crystallite size/nm	58	43	59	50

**Table S4:** Crystallite sizes derived from powder-XRD with Scherrer's equation.

## Scanning Electron Microscopy

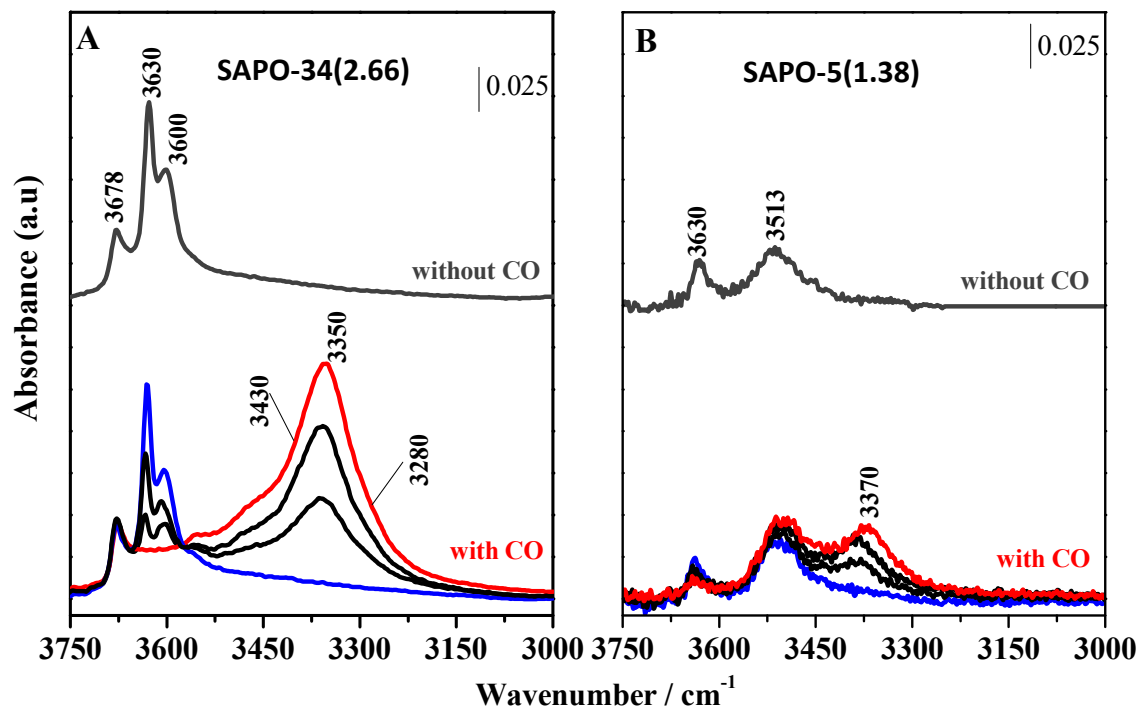


**Figure S5:** SEM image of SAPO-5(1.38).



**Figure S6:** SEM of SAPO-34(2.66).

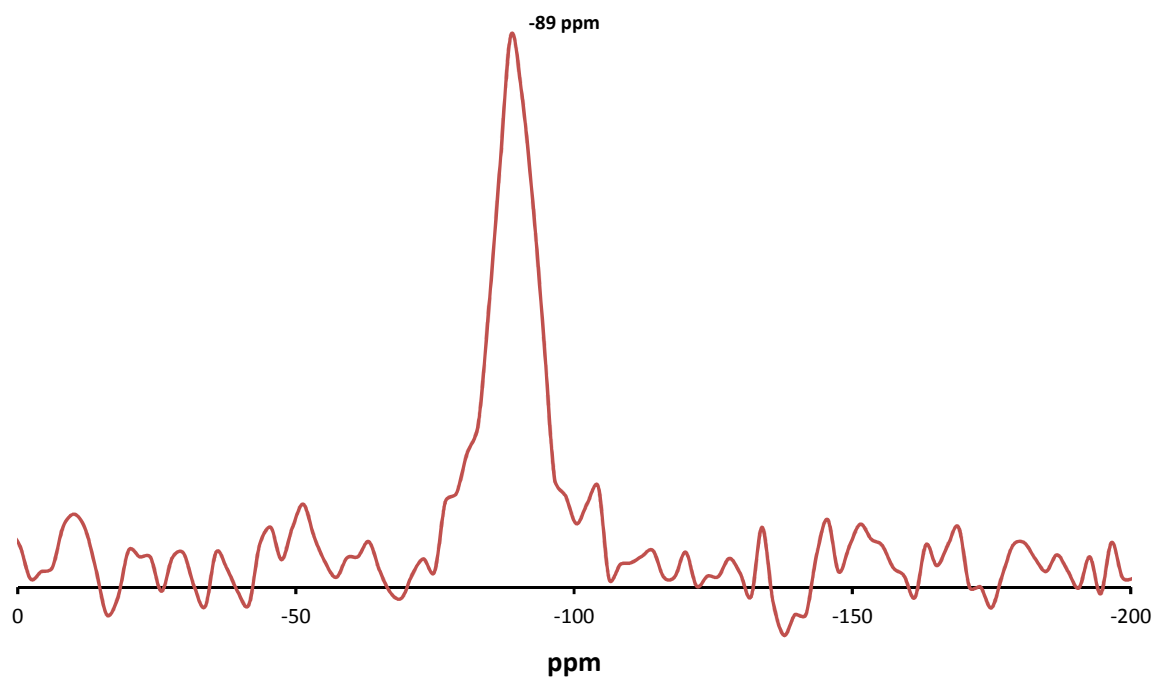
## Probe-based FTIR spectroscopy



**Figure S7:** FTIR spectra in the OH stretching region of CO adsorbed at 80 K on calcined SAPO-34(2.66) (A) and SAPO-5(1.38) (B). Decreasing CO coverages from 30 (red curves) to 0.01 (blue curves) mbar. The spectra in vacuo before CO adsorption are also reported (grey curves).

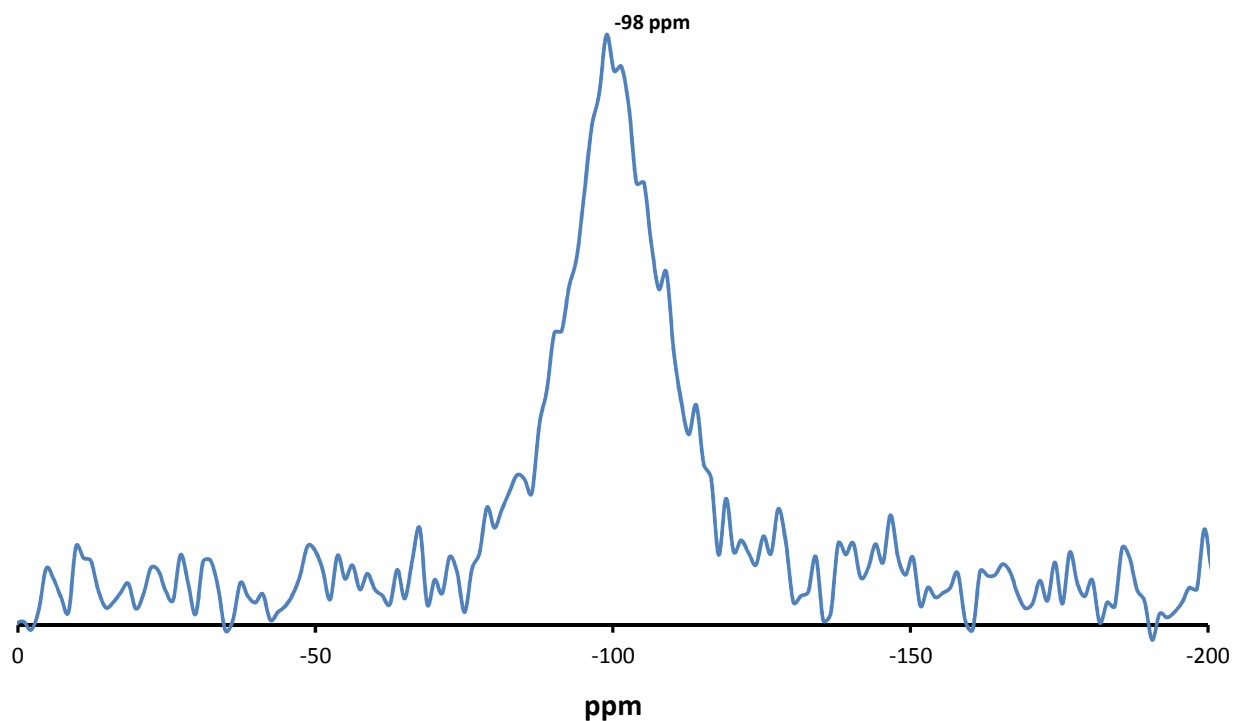
## NMR spectra

### $^{29}\text{Si}$ MAS NMR of SAPO-34(2.66)



**Figure S8:** CP-RAMP  $^{29}\text{Si}$  MAS NMR spectra of SAPO-34(2.66) at 9.4 T, 8 kHz spin rate. The spectrum is the result of 15000 scans.

### $^{29}\text{Si}$ MAS NMR of SAPO-5(1.38)



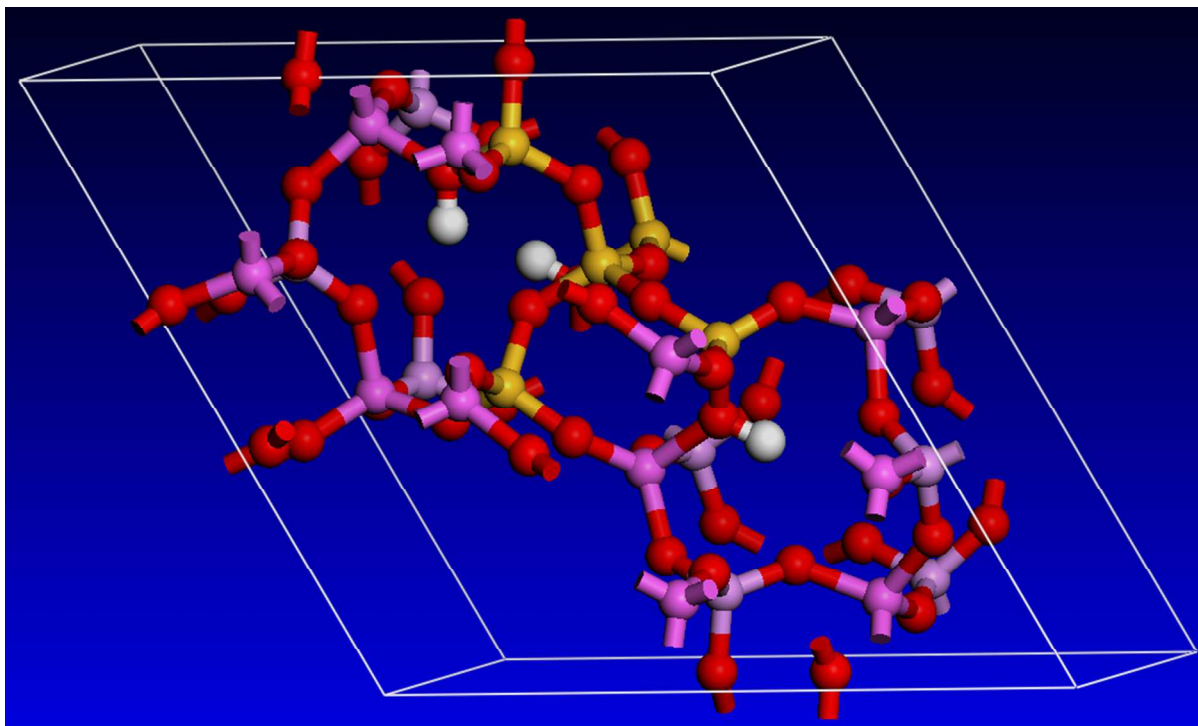
**Figure S9:** CP-RAMP  $^{29}\text{Si}$  MAS NMR spectra of SAPO-5(1.38) at 9.4 T, 8 kHz spin rate. The spectrum is the result of 25000 scans.



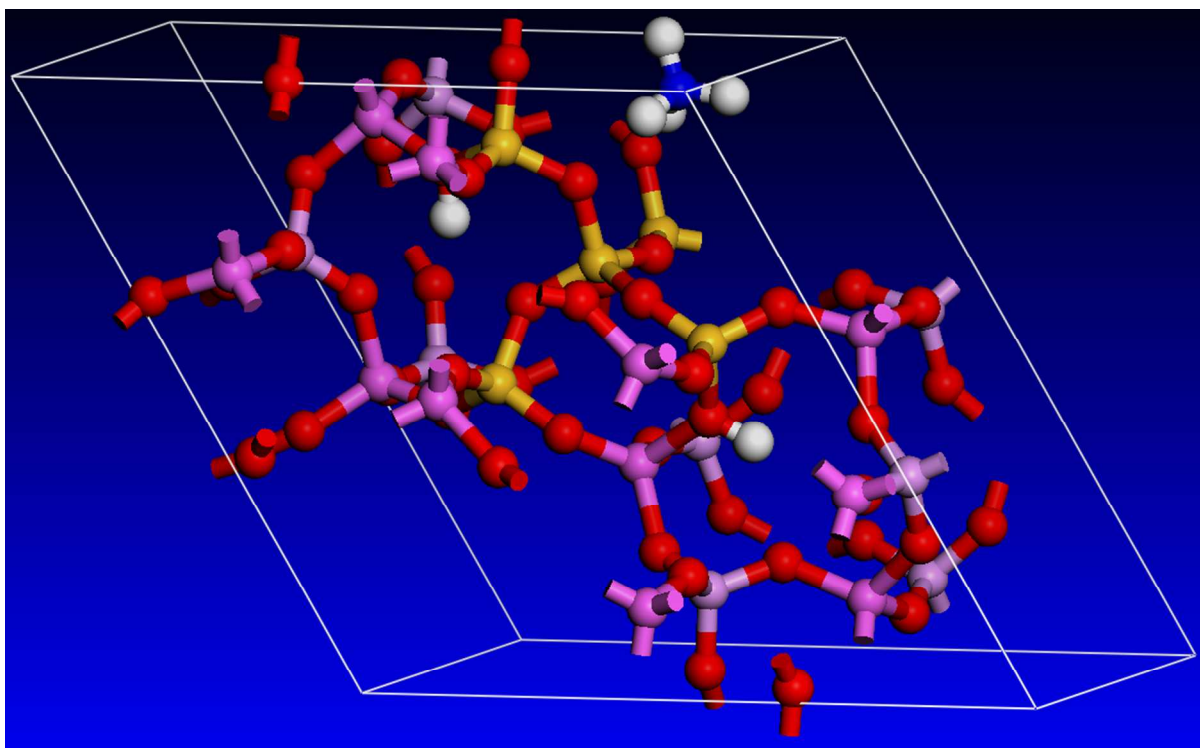
### **Computational Analysis**

Binding studies were also performed with  $\text{NH}_3$  and ethanol on the specific sites witnessed by  $^{29}\text{Si}$  NMR, to gain an insight into the acidic nature of the specific active sites and the mechanistic implications; the following equation was used to quantify the degree of interaction with the probe molecules:

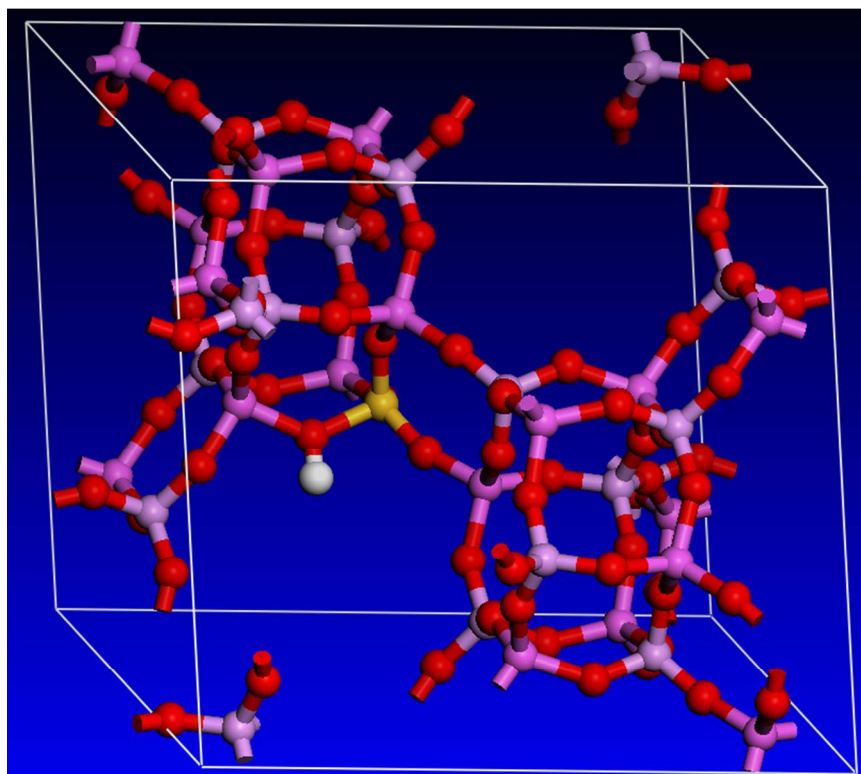
$$(4) \Delta_{\text{Binding}} = E[\text{Probe} + \text{SAPO}] - E[\text{Probe}] - E[\text{SAPO}]$$



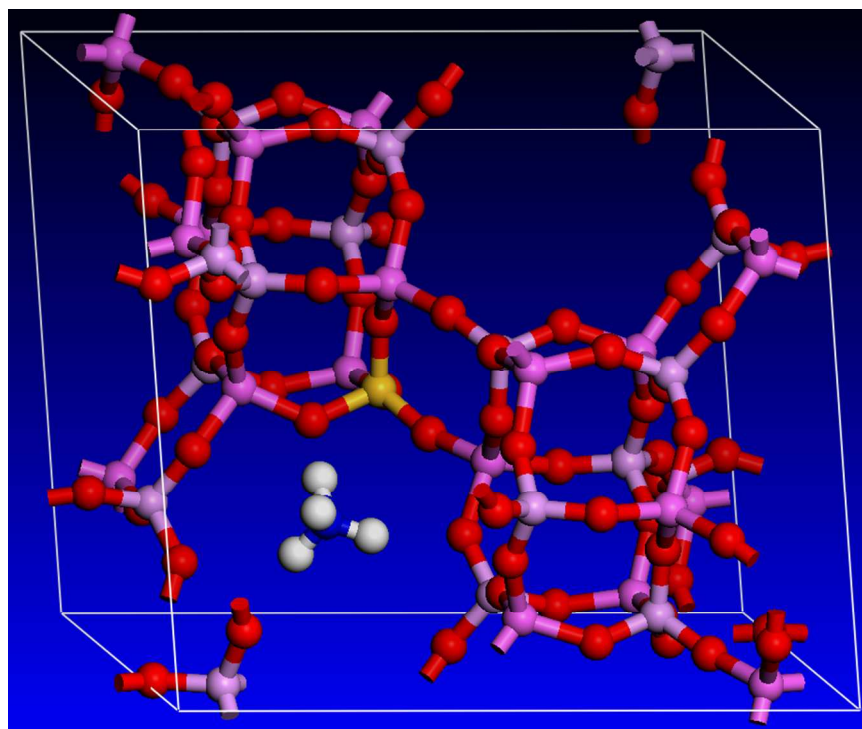
**Figure S10:** Optimised geometry of the 5-silicon island in SAPO-5.



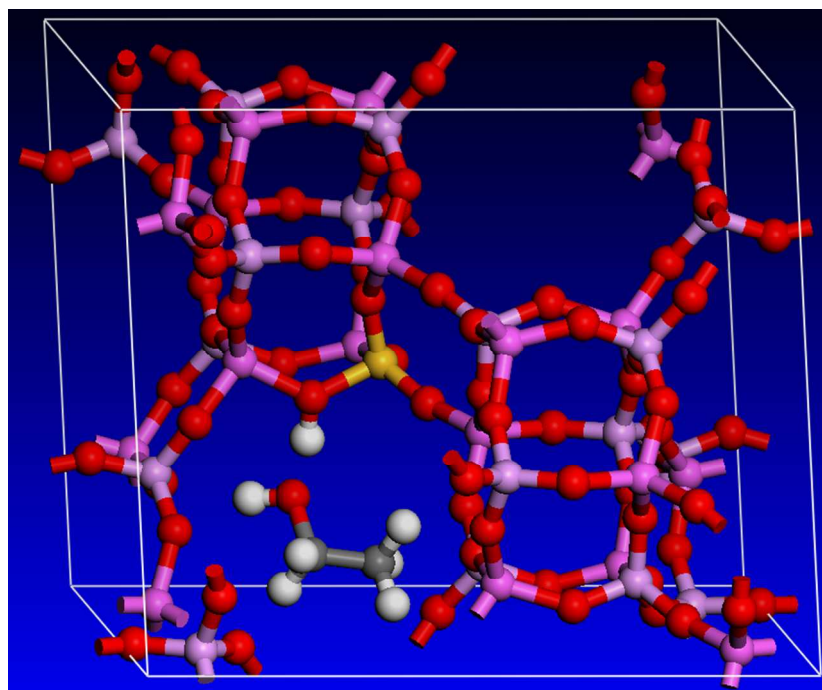
**Figure S11:** Optimised geometry of the binding of  $\text{NH}_3$  to the 5-silicon SAPO-5 species.



**Figure S12:** Optimised geometry of the isolated silicon site in SAPO-34.



**Figure S13:** The optimised geometry of the isolated silicon site in SAPO-34 binding to  $\text{NH}_3$ .



**Figure S14:** The optimised geometry of the isolated silicon site in SAPO-34 binding to ethanol.

### **Additional catalytic data**

Catalyst	Conversion/mol%			Selectivity/mol%		
	300 °C	275 °C	250 °C	300 °C	275 °C	250 °C
SAPO-5(1.38)	96	89	87	94	54	31
SAPO-34(2.66)	100	98	93	100	95	76
Blank (No catalyst)	0.3	0.3	0.3	20.8	25.3	0.0

**Table S5:** Catalytic data for dehydration of ethanol to ethylene. WHSV =  $4.38 \text{ h}^{-1}$ , He carrier gas  $50 \text{ mL min}^{-1}$ , 0.3 g catalyst. Blank reaction performed using comparable flow rates.

### **References**

- [1] Lefenfeld, M.; Raja, R.; Paterson, A. J.; Potter, M. E. WO Patent, 2010, WO/2010085708.
- [2] Lefenfeld, M.; Raja, R.; Paterson, A. J.; Potter, M. E. US Patent, 2014, US 8,759,599 B2.
- [3] Lefenfeld, M.; Raja, R.; Paterson, A. J.; Potter, M. E. EU Patent, 2010, EP2389245-A2.
- [4] Celref, version 3; LMGP (Laboratoire des Matériaux et du Génie Physique de l'Ecole Supérieure de Physique de Grenoble) Suite for Windows: Grenoble, 2000.